



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 5 : D21C 9/10		A1	(11) International Publication Number: WO 90/11403 (43) International Publication Date: 4 October 1990 (04.10.90)
(21) International Application Number: PCT/CA90/00097 (22) International Filing Date: 22 March 1990 (22.03.90)		(74) Agent: OGILVY, Renault; 1981 McGill College Avenue, Montreal, Quebec H3A 3C1 (CA).	
(30) Priority data: 594,763 23 March 1989 (23.03.89) CA		(81) Designated States: AT (European patent), BE (European patent), CH (European patent), DE (European patent), DK (European patent), ES (European patent), FR (European patent), GB (European patent), IT (European patent), LU (European patent), NL (European patent), SE (European patent), US.	
(71) Applicant (for all designated States except US): HYMAC LTD. [CA/CA]; 1867 Berlier Street, Laval, Quebec H7L 3S4 (CA).		Published <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>	
(72) Inventors; and (75) Inventors/Applicants (for US only) : BARBE, Michel [CA/CA]; 41 Place de Bohème, Candiac, Quebec J5R 3N2 (CA). GAGNE, Carole [CA/CA]; 5645 Gadbois, Trois-Rivières-Ouest, Quebec G8Y 6A6 (CA). LEDUC, Céline [CA/CA]; 862 Ste-Ursule, Trois-Rivières, Quebec G9A 5E1 (CA). DANEAULT, Claude [CA/CA]; 3805 Blvd S-Jean, Trois-Rivières, Quebec G9A 5E1 (CA).			

(54) Title: BLEACHING PROCESS FOR THE PRODUCTION OF HIGH BRIGHT PULPS

(57) Abstract

A process for the bleaching of mechanical and chemimechanical pulps which includes the steps of treating in a first stage the pulp with a reducing agent and subsequently treating the same pulp with a peroxygen compound in a second stage followed by a subsequent treatment with a peroxygen compound in a third stage.

DESIGNATIONS OF "DE"

Until further notice, any designation of "DE" in any international application whose international filing date is prior to October 3, 1990, shall have effect in the territory of the Federal Republic of Germany with the exception of the territory of the former German Democratic Republic.

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	ES	Spain	MG	Madagascar
AU	Australia	FI	Finland	ML	Mali
BB	Barbados	FR	France	MR	Mauritania
BE	Belgium	GA	Gabon	MW	Malawi
BF	Burkina Faso	GB	United Kingdom	NL	Netherlands
BG	Bulgaria	HU	Hungary	NO	Norway
BJ	Benin	IT	Italy	RO	Romania
BR	Brazil	JP	Japan	SD	Sudan
CA	Canada	KP	Democratic People's Republic of Korea	SE	Sweden
CF	Central African Republic	KR	Republic of Korea	SN	Senegal
CG	Congo	LJ	Liechtenstein	SU	Soviet Union
CH	Switzerland	LK	Sri Lanka	TD	Chad
CM	Cameroon	LJ	Luxembourg	TG	Togo
DE	Germany, Federal Republic of	MC	Monaco	US	United States of America
DK	Denmark				

1

BLEACHING PROCESS FOR THE PRODUCTION OF HIGH BRIGHT PULPS

5

This invention relates to a multistage bleaching process in which reducing agents and oxidizing agents are used sequentially to bleach mechanical and chemimechanical pulps to high brightness levels and partially remove their yellow shade.

10

15

20

25

30

35

It is well recognized by those skilled in the art of mechanical and chemimechanical pulping that the quality of mechanical and chemimechanical pulps need to be improved in terms of brightness levels, color or yellowness and rapid reversion characteristics which occur with yellowing. Therefore various processes are currently employed in the pulp and paper industry to bleach these pulps for their use in a wide variety of paper products. The oldest process uses a reducing agent such as dithionite or sodium and zinc hydrosulfite (H) to brighten or bleach the pulps. With this bleaching chemical moderate gains of 4 to 10 points are obtained. Maximum brightness levels of 68 to 70% iso can be reached with the addition of approximately 1% to 1.25% on o.d. pulp of sodium hydrosulfite. The process is usually carried out in an aqueous phase at 3 to 5% consistency, a pH of 4.5 to 6.0, a temperature of about 60°C and a retention time of up to one hour. The use of a chelating or sequestering agent such as sodium tripolyphosphate (STPP) to remove naturally occurring trace metals is recommended. This agent is being added to the pulp prior to the addition of the reducing agent or is incorporated in the bleaching solution.

Today, peroxide (P) is the most commonly employed oxidizing agent for bleaching mechanical and chemimechanical pulps. This alkaline process is normally carried out in a single stage or in a double stage. In both cases, the bleaching is done at a pulp consistency of 15 to 35%, moderate temperatures of 50 to 70°C, and retention times of 2 to 3 hours for each

1 stage. In peroxide bleaching, stabilizers such as sodium silicate and magnesium sulfate are added to the bleach liquor to prevent decomposition of the oxidizing agent. Sodium hydroxide is also used to
5 maintain an alkaline pH of 9.5 to 11 so as to increase the concentration of the perhydroxyl ion OOH^- which is believed to be the active bleaching agent. Furthermore, pulps are normally pretreated at low consistency with organic chelating agents such as
10 sodium diethylenetriamine penta-acetate (DTPA) to remove naturally occurring trace metals. Additional quantities are added in the bleach liquor to complex trace metals that are desorbed from the pulp as a result of the reaction of the bleaching agents with
15 the chromophores of the pulp. In the bleaching of commercial pulps, iso brightness of 74-76% are conventionally achieved using this process with 3% hydrogen peroxide on o.d. pulp in a single stage while values of 76-78% iso-brightness are achieved in two
20 stages in which greater retention times and higher peroxide charge are applied, i.e. 5% hydrogen peroxide on o.d. pulp.

25 Two stage bleaching of groundwood pulp using peroxide in the first stage and hydrosulfite (dithionite) in the second stage is well known and applied commercially (PH). An ISO-brightness level of 75-77% is achieved. However, much lower brightness levels are achieved when this two stage sequence is
30 reversed (HP) (Schroter, H., Wbl. Papriefab. 97, No. 23/24 (1969) p. 1023 and Joyce, P. and Mackie, M., CPPA, TAPPI International Pulp Bleaching Conference, Toronto, Canada, June 11-14, 1979, Preprint Page 116).

35 Other multistage bleaching processes have been disclosed in the literature but have not found commercial application. For instance, Loras, V. and Soteland, N. have published results for a three stage

1 bleaching sequence utilizing borohydride, peroxide and
dithionite sequentially (BPH). This sequence was
reported to yield a brightness of 88% from an initial
level of 67%, an increase of 21 points. (High
5 Brightness Bleaching of Mechanical Pulp, Norsk
Skogindustri, 10/72 p. 255). It is also known from
U.S. Patent 3,100,732 to Smedberg to use a combined
and simultaneous action of an oxidizing agent and a
reducing agent; the patentee also discloses that when
10 using a double stage sequence, one uses the oxidizing
agent first and subsequently the reducing agent.
Liebergott, N., and Heitner, C. disclosed a multistage
process for bleaching high yield and ultra-high yield
15 pulps in which the pulp is treated sequentially with a
peroxygen compound (P), a reducing compound (R) and a
final peroxygen compound (P) to achieve higher
brightness levels (Eur. Pat. Appl. EP 187,477).
Tibbling, P. also disclosed a multiperoxide stage
20 mechanical pulp bleaching process in which the pulp is
treated sequentially with hydrogen peroxide in a first
stage (P) and a second stages (P) and sodium
hydrosulfite in a third stage (H) (Eur. Pat. Appl. EP
191,756). It is claimed that higher brightness levels
25 are obtained than for those obtained for the bleaching
sequence involving hydrogen peroxide (P) followed by
sodium hydrosulfite (H).

It is an object of the present invention to
30 provide a multistage bleaching process for mechanical
and chemimechanical pulps which gives high brightness
levels to such pulps and partially remove their yellow
shade.

According to the present invention, there is
35 provided a method for the bleaching of high yield or
ultra high yield pulp which comprises the steps of
sequentially treating the lignocellulosic fibres with

1 a reducing compound and subsequently treating the same
fibres with peroxide in two successive stages.

5 In greater detail, the method or process includes
three stages where the wood pulp is subjected to
bleaching operations. The wood pulp which may be
utilized is any high yield or ultra yield pulp such as
mechanical, chemimechanical, chemithermomechanical,
groundwood, refiner mechanical pulp, thermomechanical
10 pulp, high yield and ultra high yield sulfite pulps.

15 In the first stage, the wood pulp is treated with
a reducing compound which may be chosen from many such
reducing compounds known to those skilled in the art.
During this first stage, preferred reaction conditions
include:

20 (1) a reducing compound charge of about 0.01 to
about 1.5% by weight of oven dried pulp;
(2) the presence of a chelating agent such as
DTPA or STPP;
(3) a reaction temperature of from about 60°C to
100°C;
(4) a reaction time of from about 4 to about 120
minutes;
25 (5) a pulp consistency of from 3% to about 35%
and
(6) a reaction terminating pH of about 3.5 to
about 11.0.

30 In the second stage, the pulp is bleached with a
peroxygen compound. Preferred conditions of bleaching
include:

35 (1) a peroxygen compound charge of about 0.1% to
about 5% by weight of oven dried pulp in the
presence of sodium hydroxide, sodium
silicate, magnesium sulfate and DTPA;
(2) a reaction temperature of between about 60°C
to about 100°C;

10 In the third and final bleaching stage a peroxygen compound is utilized which is similar to the one used in the second stage. The preferred reaction conditions include:

15 (1) a peroxygen compound charge of about 0.1% to about 12.0% in the presence of sodium hydroxide, sodium silicate, magnesium sulfate and DTPA;

15 (2) a reaction temperature of from about 60°C to about 100°C;

15 (3) a reaction time of about 4 minutes to about 240 minutes;

20 (4) a pulp consistency of from about 4% to about 40%; and

20 (5) a reaction terminating pH from about 7.5 to about 10.0.

25 The compounds utilized in the process of the present invention may be selected from among these well known to those skilled in the art. Thus, the reducing compounds may be chosen from commercially 30 inorganic reducing agents such as sodium or zinc hydrosulfite (dithionite), sodium or magnesium bisulfite, sodium borohydride, Borol* (a solution of sodium borohydride and sodium hydroxide), thiourea dioxide, ammonium borohydride, hydrazine and organic 35 reducing agents such as amine-boranes and phosphine-boranes. It will be noted that some of these reducing agents are sold commercially with a chelating agent mixed therewith.

* Registered Trade Mark

1 Examples of the peroxide compound utilized in the
second and third stages may include conventional
inorganic peroxides such as hydrogen and sodium
peroxide and also organic peroxides such as benzyl
5 peroxide, ditertiary-butyl peroxide and peracetic
acid.

10 The process flow diagram of figure 1 illustrates
the various steps of a continuous operation in which
pulps are bleached in multistage according to the
present invention. In the process the pulp is first
washed with a dewatering device (1) such as, but not
exclusively, a standard screw press, a displacement
15 washing screw press, a twin wire press, a disc filter
or a twin roll press. These devices allow for water
removal from the pulp slurry as well as for washing of
contaminants such as sodium sulfite, metal ions,
organic extractives, dissolved solids, etc., which are
known to impair on the bleaching reactions between the
20 bleaching agents and lignocellulosic fibres. Following
this washing stage the pulp is mixed with the
bleaching liquor containing the reducing agent. Mixing
devices (2) such as single or double shaft mixers,
refiner type mixers, high shear mixers and medium or
25 low consistency pumps can be used. It is important in
this stage of the process to disperse the bleaching
liquor uniformly onto the fibre surface so that
bleaching reactions can prevail over darkening
reactions that also occur when lignocellulosic fibres
30 are submitted to high temperature. After this pulp
mixing stage the reducing agent reacts with the pulp
in an upflow tower or steaming tube (3). A chemical
charge of 0.75 to 1.25% sodium hydrosulfite and of 0.3
to 0.5% of sodium borohydride by weight of oven dried
35 pulp are the preferred charges. A temperature between
65 to 85°C; a consistency between 3.5 to 5% for sodium
hydrosulfite and of 10 to 12% for sodium borohydride;
a reaction time of between 1 to 40 minutes is

1 preferred at this stage to favor a more effective use
of the reducing agent as it cannot be reused in the
system. A reaction terminating pH of about 4.5 to 5.0
5 for sodium hydrosulfite and of about 10.0 to 10.5 for
sodium borohydride is also recommended. Following this
first stage bleaching with a reducing agent the pulp
is dewatered and washed with a dewatering device (4)
10 such as those described previously and used in
position (1). The purpose is to wash the unreacted
reducing agents or byproducts produced from the
bleaching reactions so as to minimize its carry over
to the next bleaching stage. After this pressing and
washing stage the pulp is mixed with the peroxide
15 bleaching liquor in a mixer (5). Other devices such as
those described previously and used in position (2)
can also be used. The efficiency of the mixer is
important at this stage of the process to disperse the
bleaching liquor uniformly onto the fibre surface so
that oxidizing bleaching reactions of the chromophoric
20 groups on the lignocellulosic fibres occur and prevail
over darkening reactions that also occur when pulps
are submitted to high temperatures. We show in figure
1 a mixer (5) which allows for the addition of steam
and the peroxide bleaching liquor simultaneously.
25 Following this mixing stage the pulp is transferred to
a bleaching tower (6). The most preferred charge of
the peroxygen compound in this second stage bleaching
is in amount equal to the charge of the last bleaching
tower or to one third of the charge of the last
30 bleaching tower. Sodium hydroxide, sodium silicate and
magnesium sulfate are preferably added in charge
ranges of 0.5-3.0%, 0.0 to 3.0% and 0.01-0.05%
respectively. It is also preferable to add small
35 amounts of DTPA between 0.1-0.4%. All these components
stabilize the peroxygen compound, in the form of the
perhydroxyl ion, initiate and maintain a stable
bleaching reaction. In a commercial operation the
peroxide bleaching liquor mixed with the pulp at this

1 stage can be either prepared from fresh commercial components dissolved in water in separate tanks or it can be a residual bleaching liquor solution from the last stage bleaching tower (9). We have found from
5 mass balance calculations that this latter is preferable to minimize the operating and bleaching cost of the process disclosed in this application. The size of the second bleaching tower (6) is to be determined considering the production rate, reaction
10 time and pulp consistency selected or desired. We have found that a consistency in the 10-12% range, a retention time of 60 to 90 minutes and a temperature of 65 to 70°C are preferable to minimize the bleaching cost of the process disclosed. In figure 1 we show a
15 schematic of a tower which is discharged with a medium consistency pump so as to have an operation with an efficient control over the bleaching conditions.

Following this second stage bleaching with an
20 oxidizing agent the pulp is dewatered and washed with a dewatering device (7) such as those described previously and used in position (1) and (4). The purpose is to wash the byproducts produced from the bleaching reactions which occurred in the second stage
25 bleaching tower, avoid their carry over to the next bleaching stage and eliminate these from the bleach plant with an adequate white water recirculation strategy. After this pressing and washing stage the pulp is mixed with the peroxide bleaching liquor in a
30 mixer (8). The mixer used and its efficiency are important at this stage for the same reasons as those elaborated previously above. Following this mixing stage the pulp is transferred to a bleaching tower (9). The preferred charge of the peroxygen compound in
35 this third stage bleaching is 3 to 10% by weight of oven dried pulps. Sodium hydroxide, sodium silicate and magnesium sulfate are preferably added in charge ranges of 0.25-0.3%, 0.01% to 3.0% and 0.01-0.05%

1 respectively. It is also preferable to add small
5 amounts of DTPA between 0.2-0.4%. In a commercial
10 operation it is preferable in this last bleaching
15 stage that fresh peroxide bleaching liquor be used and
20 mixed with the pulp. This bleaching liquor is normally
25 prepared from fresh commercial components which are
30 dissolved in water in separate tanks. In addition to
35 this fresh liquor, a small quantity of the residual
40 bleaching liquor solution from the same tower (9) can
45 also be used. The residual bleaching liquor is
50 recovered with the last pair of dewatering presses (11
55 and 12). We have found that high charges of peroxide
60 are required in this last bleaching tower to achieve
65 high brightness levels. The size of the third
70 bleaching tower (9) is to be determined considering
75 the production rate, reaction time and pulp
80 consistency selected or desired. We have found that a
85 consistency in the 20-35% range is preferable to have
90 high effective concentrations of the oxidizing agents
95 so as to minimize the bleaching cost of the process
100 disclosed.

1 In figure 1 we show a schematic of a tower which
2 is discharged in a transfer chest (10) with a screw
3 conveyer. This device allows for a positive
4 displacement out of the tower so as to provide an
5 efficient control over the operating and bleaching
6 conditions of the pulp in the tower.

1 Following this third stage bleaching with an
2 oxidizing agent the pulp is washed and dewatered with
3 dewatering devices, (11) and (12), such as those
4 described previously. At this stage it is important to
5 add fresh water in the transfer chest (10) to wash the
6 pulp by dilution and minimize brightness reversion
7 subsequently. After the final stage of the bleaching
8 process the pulp is pressed so as to recover the
9 unreacted peroxide bleaching liquor and to reuse it in

1 the process as shown in figure 1. This white-water
recirculation strategy and counter current washing
lowers the operating cost of the bleaching process
disclosed. The addition of sulfuric acid in the
5 transfer chest (10) or the addition of SO₂ in the
fluffer (13) is also desirable to lower the aqueous
solution pH to about 6 to minimize brightness
reversion subsequently.

Having thus generally described the invention,
10 reference will be made to the following examples;

EXAMPLE 1.

15 A commercial spruce balsam chemithermomechanical
pulp from an Eastern Canadian mill was washed with
0.5% diethylenetriaminepentaacetate (DTPA) for 30
minutes at 60°C and 3% consistency to eliminate metal
ions which impair the bleaching reactions. Following
20 this treatment, the pulp was pressed to 25%
consistency and bleached. The experimental conditions
and chemical charges are given in Table 1.

25 The bleaching chemicals were mixed by hand with a
20-g pulp sample, while the pulp consistency was
simultaneously adjusted with demineralized water.
Subsequently, the bags were sealed and immersed in a
thermostatically controlled bath for the bleaching
reactions to occur. After bleaching, the pulps were
neutralized to destroy the bleaching agents and to
30 adjust the pulp pH to minimize brightness reversion.
For hydrogen peroxide bleaching, sodium metabisulfide
was used, while sulfuric acid was used for the other
bleaching agents.

35 The pulps were neutralized by diluting the pulp to
3% consistency with the neutralizing agent, mixing the
slurry for 5 minutes, and pressing the pulp to 18%
consistency. After neutralization, two samples of 3.5g

1 each were used to make the handsheets. The pulps were
disintegrated for 2 minutes at a consistency of
approximately 0.3%. The sheets were made with
5 demineralized water on a British handsheet machine
following the procedures prescribed by the Canadian
Pulp and Paper Association. The sheets were pressed
for 2 minutes at 50 psig and dried for 24 h at 23°C
and 50% RH. The brightness was measured with an
Elrepho spectrophotometer. Reflectance measurements
10 with Filter Nos. 8, 9, 10, and 11 were made and used
to calculate the color coordinates (CIE LAB) reference
system. ISO brightness reported are the reflectance
values at 457 nm using filter No. 8.

15 In the multistage bleaching experiments, each
stage was similar to the single stage. However, the
two-stage experiments were carried out with 30-g pulp
samples, and 40-g samples were used for three stages.
20 In all cases, a 7-g sample was taken at the end of
each stage and was processed to obtain brightness
values.

25 The results in Table I show the superiority of the
multistage bleaching process disclosed in the present
invention compared to the bleaching processes which
constitute the prior art. High brightness values are
achieved (ISO-brightness and L*) and a great deal of
30 the yellow shade of the pulps is removed (B* values)
while the pulps have less greenish shade than those
bleached with peroxide only (P). These benefits remain
after reversion. It can also be observed that for the
bleaching process disclosed less peroxide is consumed
to achieve higher brightness levels.

1

EXAMPLE 2.

A commercial spruce balsam chemithermomechanical pulp was pretreated and bleached following the experimental procedures described in example 1 and under the chemical charges and bleaching conditions given in Table 2. The results in Table 2 show the superiority of the multistage bleaching process disclosed in the present invention compared to other multistage bleaching sequences; peroxide-reducing agent-peroxide (PRP) and peroxide-peroxide-sodium hydrosulfite (PPH). With the sequences sodium hydrosulfite-peroxide-peroxide (HPP) and sodium borohydride-peroxide-peroxide (BPP) higher ISO-brightness values are obtained for a given total peroxide addition level while less peroxide is consumed in the process. Inversely at a constant peroxide consumption level lower ISO-brightness values are obtained with the bleaching procedures of the prior art compared with the process disclosed in this application. In addition to higher brightness values it can be seen from Table 2 that low B* values are obtained which indicate that the pulp bleached following the process disclosed is less yellow than the control pulp, as well as the pulp bleached with hydrogen peroxide only or upon bleaching with the procedures described in the prior art.

30

EXAMPLE 3.

A commercial spruce balsam chemithermomechanical pulp was pretreated and bleached following the experimental procedures described in example 1. In this series of experiments the pulp was bleached under different charges of the reducing agent in the first stage. The charges used were from 0.01% to 0.5% while the total peroxide charge was kept constant at 5%. The

1 results in Table 3 show that higher brightness values
are obtained with increasing charges of the reducing
agent. It can be observed that an optimum charge
5 between 0.1 to 0.3% is desirable. Progressively lower
B* values are obtained with the addition of the
reducing agent therefore eliminating a great deal of
the yellowness of the pulp.

10

EXAMPLE 4.

15 A commercial spruce balsam chemithermomechanical
pulp was pretreated and bleached following the
experimental procedures described in example 1. In
this series of experiments the pulp was bleached under
a given charge of 0.3% of the reducing agent, sodium
20 borohydride, in the first stage while increasing
charges of peroxide up to 5% by weight on oven dried
pulp were added in the second and third stages. The
results in Table 4 show that higher brightness values
are obtained with increasing charges of peroxide in
the second and third stages. It can be observed that
25 small brightness gains are realized with charge levels
slightly in excess of 3% so that preferred conditions
would be for an addition level of 4 to 5% in peroxide
o.d. weight when sodium borohydride is used.
Progressively lower B* values are obtained with the
addition of peroxide therefore eliminating a great
deal of the yellowness of the pulp.

30

EXAMPLE 5.

35 A commercial spruce balsam chemithermomechanical
pulp was pretreated and bleached following the
experimental procedures described in example 1. In
this series of experiments the pulp was bleached using
a constant charge of 0.5% sodium hydrosulfite as the

1 reducing agent in the first stage. In the second and
thirst stages progressively increasing peroxide charges
were added from 1% to 8% o.d. weight o.d. pulp. The
results in Table 5 show that higher brightness values
5 are obtained with increasing charges of peroxide in
the second and third stages. It can be observed that
smooth increases are obtained up to 8% added peroxide
allowing for high brightness levels and appreciable
pulp yellowness removal.

10

EXAMPLE 6.

15 A commercial spruce balsam chemithermomechanical
pulp was pretreated and bleached following the
experimental procedures described in example 1. In
this series of experiments the pulp was bleached using
a constant charge of 1.0% sodium hydrosulfite as the
reducing agent in the first stage. In the second and
20 third stages progressively increasing charges of
peroxide were added from 1% to 8% o.d. weight on pulp.
The results in Table 5 show that higher brightness
values are obtained with increasing charges of
peroxide in the second and third stages. It can be
observed that smooth increases are obtained up to 8%
25 added peroxide allowing for high brightness levels and
appreciable pulp yellowness removal. It can be
appreciated that higher brightness levels are achieved
compared to example 5 so that preferred reducing agent
30 charges are 1.0 to 1.25% o.d. weight on pulp.

35 It will be understood that the above described
embodiments are for purposes of illustration only and
that changes and modifications may be made thereto
without departing from the spirit and scope of the
invention.

TABLE 1:		BLEACHING CHEMICALS AND SEQUENCES										
		CHEMICAL CHARGES AND BLEACHING CONDITIONS	UNBL. PULP	HYDRO- SULFITE		PEROXIDE- HYDROSULFITE			BLEACHING PROCESS DISCLOSED			
				(H)	(P)	(PH)	(PH)	PEROXIDE (PP)	(HPP)	(HPP)	(BPP)	(BPP)
5	FIRST STAGE											
	Na2SiO3	1		—	3.00	3.00	3.00	3.00	—	—	—	—
	MgSO4	1		—	0.05	0.05	0.05	0.05	—	—	—	—
	NaOH	1		—	3.00	1.60	1.80	1.80	—	—	—	—
	D.T.P.A.	1		0.40	0.40	0.40	0.40	0.40	0.40	0.40	0.40	0.40
	H2O2 ADDED	1		—	3.00	2.50	4.00	2.50	—	—	—	—
	NaBH4	1		—	—	—	—	—	—	—	—	—
10	Na2SO4	1		1.00	—	—	—	—	—	—	0.30	0.30
	CONSISTENCY	1		5.0	15.0	10.0	10.0	10.0	1.00	1.00	—	—
	TEMPERATURE	C		70	70	70	70	70	5.0	5.0	10.0	10.0
	RETENTION TIME	min.		30	90	90	90	90	70	70	70	70
	pH (INITIAL)	—		5.5	11.0	11.0	11.0	11.0	5.4	5.3	11.7	11.5
	pH (FINAL)	—		5.0	9.6	8.4	8.5	9.5	4.9	5.0	10.4	10.4
	SECOND STAGE											
15	Na2SiO3	1		—	—	3.00	3.00	3.00	3.00	3.00	3.00	3.00
	MgSO4	1		—	—	0.05	0.05	0.05	0.05	0.05	0.05	0.05
	NaOH	1		—	—	1.54	1.74	2.26	1.39	1.39	1.39	1.39
	D.T.P.A.	1		—	0.40	0.40	0.40	0.40	0.40	0.40	0.40	0.40
	H2O2 ADDED	1		—	—	2.50	2.50	4.00	1.52	1.52	2.50	2.50
	Na2SO4	1		1.00	1.00	—	—	—	—	—	—	—
	CONSISTENCY	1		—	5.0	5.0	20.0	10.0	10.0	10.0	10.0	10.0
	TEMPERATURE	C		70	70	70	70	70	70	70	70	70
	RETENTION TIME	min.		30	30	90	90	90	90	90	90	90
20	pH (INITIAL)	—		—	5.4	5.4	11.0	10.9	10.8	11.1	11.1	11.0
	pH (FINAL)	—		—	4.2	4.4	10.7	8.7	8.8	10.1	10.1	10.5
	THIRD STAGE											
25	Na2SiO3	1		—	—	—	—	3.00	3.00	3.00	3.00	3.00
	MgSO4	1		—	—	0.05	0.05	0.05	0.05	0.05	0.05	0.05
	NaOH	1		—	—	1.73	2.00	1.62	1.62	1.62	1.62	1.62
	D.T.P.A.	1		—	—	0.40	0.40	0.40	0.40	0.40	0.40	0.40
	H2O2 ADDED	1		—	—	2.52	4.00	1.52	2.50	2.50	2.50	2.50
	CONSISTENCY	1		—	—	28.0	28.0	28.0	28.0	28.0	28.0	28.0
	TEMPERATURE	C		—	—	70	70	70	70	70	70	70
	RETENTION TIME	min.		—	—	92	98	92	92	92	92	92
	pH (INITIAL)	—		—	—	11.1	11.1	11.1	11.1	11.1	11.1	11.1
	pH (FINAL)	—		—	—	18.5	18.6	18.5	18.5	18.5	18.5	18.5
	TOTAL											
30	H2O2 (ADDED)	1		—	3.00	2.50	4.00	5.00	5.00	8.00	3.00	3.00
	H2O2 (RESIDUAL)	1		—	0.79	1.32	2.46	2.18	2.79	5.56	1.65	2.05
	H2O2 (CONSUMED)	1		—	2.21	1.18	1.34	2.82	2.21	2.44	1.34	2.15
	OPTICAL PROPERTIES											
	BEFORE REVERSION :											
	BRIGHTNESS (ISO-457nm)	1	62.5	68.5	77.1	76.4	77.4	78.5	79.0	80.5	77.8	78.2
	L*	—	88.1	91.4	95.1	94.5	94.8	95.3	95.8	95.3	95.1	95.8
35	A*	—	-8.37	-8.98	-2.16	-1.88	-1.95	-2.65	-1.97	-2.83	-2.67	-2.28
	B*	—	9.25	9.68	9.16	8.61	8.48	8.33	7.43	6.68	8.35	7.98
	AFTER REVERSION :											
	BRIGHTNESS (ISO-457nm)	1	61.9	67.5	75.7	74.5	75.0	76.6	77.7	78.4	75.5	77.8
	L*	—	88.0	91.1	94.5	94.2	94.2	94.4	94.6	95.0	94.6	94.1
	A*	—	-8.37	-1.14	-3.80	-1.94	-1.75	-3.88	-1.88	-2.81	-2.72	-2.78
	B*	—	9.64	10.00	9.18	9.48	8.98	7.83	8.88	7.59	6.92	7.39

1 TABLE 2: BLEACHING CHEMICALS AND SEQUENCE

CHEMICAL CHARGES AND BLEACHING CONDITIONS	UXBL. PULP	BLEACHING PROCESS DISCLOSED											
		(PP)	(PP)	(PBP)	(PBP)	(PHP)	(PHP)	(PPH)	(PPH)	(BPP)	(BPP)	(HPP)	(HPP)
5 FIRST STAGE													
Na2SiO3	I	3.88	3.88	3.82	3.88	3.88	3.88	3.88	3.88	-	-	-	-
MgSO4	I	8.85	8.85	8.85	8.85	8.85	8.85	8.85	8.85	-	8.88	-	-
NaOH	I	1.88	1.88	1.68	1.68	1.68	1.68	1.88	1.88	1.88	1.88	-	-
D.T.P.A.	I	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48
H2O2 ADDED	I	2.58	1.52	2.58	-	2.58	-	2.58	-	-	-	-	-
NaBH4	I	-	-	-	-	-	-	-	-	8.38	8.38	-	-
Na2S2O4	I	-	-	-	-	-	-	-	-	-	-	8.58	8.58
10 CONSISTENCY	I	18.8	18.8	18.8	18.8	18.8	18.8	18.8	18.8	18.8	18.8	18.8	18.8
TEMPERATURE	C	78	78	78	78	78	78	78	78	78	78	78	78
RETENTION TIME	min.	98	98	98	98	98	98	98	98	28	28	38	38
pH (INITIAL)	-	11.8	11.8	11.8	11.8	11.8	11.8	11.8	11.8	11.5	11.5	5.4	5.2
pH (FINAL)	-	9.5	9.5	8.6	8.6	8.4	8.4	8.7	8.7	10.4	10.4	5.2	5.4
SECOND STAGE													
15 Na2SiO3	I	3.88	3.88	-	-	-	-	3.88	3.88	3.88	3.88	3.88	3.88
MgSO4	I	8.85	8.85	-	-	-	-	8.85	8.85	8.85	8.85	8.85	8.85
NaOH	I	1.84	1.54	1.88	1.88	-	-	1.78	1.78	1.78	1.39	1.39	1.74
D.T.P.A.	I	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48
H2O2 ADDED	I	2.58	1.53	-	1.72	-	1.72	2.58	1.85	2.58	2.27	2.58	2.25
NaBH4	I	-	-	8.38	8.38	-	-	-	-	-	-	-	-
Na2S2O4	I	-	-	-	-	8.58	8.58	-	-	-	-	-	-
CONSISTENCY	I	28.8	28.8	18.8	18.8	5.8	5.8	28.8	28.8	18.8	18.8	18.8	18.8
TEMPERATURE	C	78	78	78	78	78	78	78	78	78	78	78	78
RETENTION TIME	min.	98	98	28	28	38	38	98	98	98	98	98	98
pH (INITIAL)	-	11.8	11.8	12.2	12.2	5.4	5.4	11.8	11.8	11.8	11.8	11.1	11.1
pH (FINAL)	-	10.7	10.7	11.0	11.0	4.4	4.4	10.3	10.3	10.5	10.5	8.6	8.6
THIRD STAGE													
25 Na2SiO3	I	-	-	3.88	3.88	3.88	3.88	-	-	3.88	3.88	3.88	3.88
MgSO4	I	-	-	8.85	8.85	8.85	8.85	-	-	8.85	8.85	8.85	8.85
NaOH	I	-	-	1.25	1.25	1.88	1.88	-	-	1.28	1.28	1.75	1.75
D.T.P.A.	I	-	-	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48	8.48
H2O2 ADDED	I	-	-	2.58	1.73	2.58	1.73	-	1.85	2.58	2.58	2.58	2.25
Na2S2O4	I	-	-	-	-	-	-	8.58	8.58	-	2.28	-	-
CONSISTENCY	I	-	-	28.8	28.8	28.8	28.8	5.8	5.8	28.8	28.8	28.8	28.8
TEMPERATURE	C	-	-	78	78	78	78	78	78	78	78	78	78
RETENTION TIME	min.	-	-	98	98	98	98	38	38	98	98	98	98
pH (INITIAL)	-	-	-	11.8	11.8	11.8	11.8	5.5	5.5	11.1	11.1	11.8	11.8
pH (FINAL)	-	-	-	11.8	11.8	9.6	9.6	5.5	5.5	10.5	10.5	10.4	10.4
30 TOTAL													
H2O2 (ADDED)	I	5.88	3.25	5.88	3.45	5.88	3.45	5.88	3.78	5.88	4.55	5.88	4.58
H2O2 (RESIDUAL)	I	2.18	8.93	2.43	1.45	2.62	1.45	2.57	1.78	2.85	2.55	2.97	2.58
H2O2 (CONSUMED)	I	2.82	2.88	2.57	2.88	2.38	2.88	2.43	2.88	2.15	2.82	2.83	2.88
OPTICAL PROPERTIES													
35 BEFORE REVERSION :													
BRIGHTNESS (ISO-457nm) I	-	62.8	78.5	75.9	79.8	78.9	77.5	76.7	78.8	77.8	78.2	78.2	78.7
L*	-	87.3	95.3	94.6	94.9	95.8	94.8	94.7	94.9	94.4	95.8	95.2	95.1
A*	-	-8.74	-2.65	-2.68	-1.86	-1.98	-2.82	-1.98	-1.91	-1.75	-2.28	-2.88	-2.38
B*	-	8.37	8.33	9.17	7.28	8.18	8.25	8.68	7.99	8.23	7.98	7.82	8.88
AFTER REVERSION :													
BRIGHTNESS (ISO-457nm) I	-	61.9	76.6	74.6	77.2	-	75.3	-	76.9	-	77.8	-	78.2
L*	-	87.4	94.4	93.8	93.7	-	94.4	-	94.7	-	94.1	-	95.1
A*	-	-1.25	-3.88	-3.18	-2.16	-	-1.78	-	-1.95	-	-2.78	-	-1.93
B*	-	8.33	8.33	9.17	7.28	8.18	8.25	8.68	7.99	8.23	7.98	7.82	8.88

1 TABLE 3: CHEMICAL CHARGES AND BLEACHING CONDITIONS FOR
THE SEQUENCE SODIUM BOROHYDRIDE-PEROXIDE-PEROXIDE (BPP)

FIRST STAGE								
5	NaOH	%	8.83	8.18	8.17	8.33	8.88	8.67
	D.T.P.A.	%	8.48	8.48	8.48	8.48	8.48	8.48
	NaBH4	%	8.81	8.83	8.85	8.18	8.38	8.58
	CONSISTENCY	%	18.8	18.8	18.8	18.8	18.8	18.8
	TEMPERATURE	°C	78	78	78	78	78	78
	RETENTION TIME	min.	28	28	28	28	28	28
	pH (INITIAL)	-	8.3	9.7	18.3	18.9	11.5	11.8
	pH (FINAL)	-	7.8	9.1	9.3	9.8	18.4	11.8
SECOND STAGE								
10	Na2SiO3	%	3.88	3.88	3.88	3.88	3.88	3.88
	MgSO4	%	8.85	8.85	8.85	8.85	8.85	8.85
	NaOH	%	1.74	2.89	1.56	1.39	1.39	1.22
	D.T.P.A.	%	8.48	8.48	8.48	8.48	8.48	8.48
	H2O2 ADDED	%	2.58	2.58	2.58	2.58	2.58	2.58
	CONSISTENCY	%	18.8	18.8	18.8	18.8	18.8	18.8
	TEMPERATURE	°C	78	78	78	78	78	78
15	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5	1.5
	pH (INITIAL)	-	11.8	11.8	11.8	11.8	11.8	11.8
	pH (FINAL)	-	9.1	8.8	9.5	9.5	18.5	18.2
THIRD STAGE								
20	Na2SiO3	%	3.88	3.88	3.88	3.88	3.88	3.88
	MgSO4	%	8.85	8.85	8.85	8.85	8.85	8.85
	NaOH	%	1.25	1.88	8.75	1.25	1.88	1.88
	D.T.P.A.	%	8.48	8.48	8.48	8.48	8.48	8.48
	H2O2 ADDED	%	2.58	2.58	2.58	2.58	2.58	2.58
	CONSISTENCY	%	28.8	28.8	28.8	28.8	28.8	28.8
	TEMPERATURE	°C	78	78	78	78	78	78
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5	1.5
	pH (INITIAL)	-	11.1	11.8	11.8	11.2	11.1	11.8
	pH (FINAL)	-	18.1	18.3	18.4	18.5	18.5	18.6
TOTAL								
25	H2O2 (ADDED)	%	5.88	5.88	5.88	5.88	5.88	5.88
	H2O2 (RESIDUAL)	%	2.38	2.34	2.41	2.48	2.85	3.19
	H2O2 (CONSUMED)	%	2.62	2.66	2.59	2.52	2.15	1.81
OPTICAL PROPERTIES								
30	BEFORE REVERSION :							
	BRIGHTNESS (ISO-457nm) %		62.8	77.5	77.2	77.8	78.5	78.2
	L*	-	87.3	93.8	95.8	95.8	95.3	95.8
	A*	-	-8.74	-2.71	-2.75	-2.75	-2.92	-2.20
	B*	-	8.37	8.77	8.54	8.52	8.25	7.98
								7.64
35	AFTER REVERSION :							
	BRIGHTNESS (ISO-457nm) %		61.9	75.9	76.8	76.5	77.8	77.8
	L*	-	87.4	94.1	94.1	94.1	94.1	93.8
	A*	-	-1.25	-3.81	-3.81	-2.49	-2.93	-2.78
	B*	-	8.73	8.19	8.19	7.39	7.39	6.94

1

TABLE 4: CHEMICAL CHARGES AND BLEACHING CONDITIONS FOR THE SEQUENCE SODIUM BOROHYDRIDE-PEROXIDE-PEROXIDE (BPP)

FIRST STAGE							
5	NaOH	1	1.00	1.00	1.00	1.00	
	D.T.P.A.	1	0.40	0.40	0.40	0.40	
	NaBH4	1	0.30	0.30	0.30	0.30	
	CONSISTENCY	1	10.0	10.0	10.0	10.0	
	TEMPERATURE	C	70	70	70	70	
	RETENTION TIME	min.	20	20	20	20	
	pH (INITIAL)	-	11.5	11.5	11.7	11.5	
	pH (FINAL)	-	10.0	10.3	10.4	10.4	
SECOND STAGE							
10	Na2S103	1	3.00	3.00	3.00	3.00	
	MgSO4	1	0.05	0.05	0.05	0.05	
	NaOH	1	0.70	1.22	1.39	1.39	
	D.T.P.A.	1	0.40	0.40	0.40	0.40	
	H2O2 ADDED	1	0.50	1.00	1.50	2.50	
	CONSISTENCY	1	10.0	10.0	10.0	10.0	
	TEMPERATURE	C	70	70	70	70	
15	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	
	pH (INITIAL)	-	11.0	11.0	11.1	11.0	
	pH (FINAL)	-	10.0	10.1	10.1	10.3	
THIRD STAGE							
20	Na2S103	1	3.00	3.00	3.00	3.00	
	MgSO4	1	0.05	0.05	0.05	0.05	
	NaOH	1	1.15	1.50	1.00	1.00	
	D.T.P.A.	1	0.40	0.40	0.40	0.40	
	H2O2 ADDED	1	0.50	1.00	1.50	2.50	
	CONSISTENCY	1	10.0	10.0	10.0	10.0	
	TEMPERATURE	C	70	70	70	70	
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	
	pH (INITIAL)	-	11.1	11.0	11.1	11.1	
	pH (FINAL)	-	10.7	10.7	10.5	10.3	
TOTAL							
25	H2O2 (ADDED)	1	1.00	2.00	3.00	5.00	
	H2O2 (RESIDUAL)	1	-	0.90	1.66	2.85	
	H2O2 (CONSUMED)	1	-	1.10	1.34	2.15	
OPTICAL PROPERTIES							
30	BEFORE REVERSION :						
	BRIGHTNESS (ISO-457nm)%	62.0	74.3	76.9	77.8	78.2	
	L*	-	87.3	94.2	94.6	95.1	
	A*	-	-0.74	-2.42	-2.51	-2.67	
	B*	-	8.37	9.49	8.68	8.35	
35	AFTER REVERSION :						
	BRIGHTNESS (ISO-457nm)%	61.9	73.3	75.1	76.5	77.0	
	L*	-	87.4	93.5	93.9	94.8	
	A*	-	-1.25	-3.01	-2.69	-2.72	
	B*	-	8.73	9.28	8.47	8.06	

1 TABLE 5: CHEMICAL CHARGES AND BLEACHING CONDITIONS FOR
THE SEQUENCE SODIUM HYDROSULFITE-PEROXIDE-PEROXIDE (HPP)

FIRST STAGE							
5	D.T.P.A.	I	8.48	8.48	8.48	8.48	8.48
	Na2S2O4	I	8.58	8.58	8.58	8.58	8.58
	CONSISTENCY	I	5.8	5.8	5.8	5.8	5.8
	TEMPERATURE	C	78	78	78	78	78
	RETENTION TIME	hr.	8.5	8.5	8.5	8.5	8.5
	pH (INITIAL)	-	5.4	5.4	5.5	5.4	5.2
	pH (FINAL)	-	4.8	4.5	4.7	5.2	5.1
SECOND STAGE							
10	Na2S1O3	I	3.88	3.88	3.88	3.88	3.88
	MgSO4	I	8.05	8.05	8.05	8.05	8.05
	NaOH	I	8.70	1.22	1.39	1.74	2.89
	D.T.P.A.	I	-	8.48	8.48	8.48	8.48
	H2O2 ADDED	I	8.58	1.88	1.58	2.58	4.88
	CONSISTENCY	I	18.8	18.8	18.8	18.8	18.8
	TEMPERATURE	C	78	78	78	78	78
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5
	pH (INITIAL)	-	10.9	11.8	11.8	11.1	11.0
	pH (FINAL)	-	9.7	8.7	8.5	8.6	8.8
THIRD STAGE							
15	Na2S1O3	I	3.88	3.88	3.88	3.88	3.88
	MgSO4	I	8.05	8.05	8.05	8.05	8.05
	NaOH	I	8.75	1.23	1.58	1.75	2.88
	D.T.P.A.	I	8.48	8.48	8.48	8.48	8.48
	H2O2 ADDED	I	8.58	1.88	1.58	2.58	4.88
	CONSISTENCY	I	18.8	18.8	18.8	18.8	18.8
	TEMPERATURE	C	78	78	78	78	78
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5
	pH (INITIAL)	-	11.8	11.8	11.8	11.8	11.8
	pH (FINAL)	-	10.3	9.8	9.8	10.4	10.0
TOTAL							
20	H2O2 (ADDED)	I	1.88	2.88	3.88	5.88	8.88
	H2O2 (RESIDUAL)	I	8.26	8.78	1.45	2.97	4.45
	H2O2 (CONSUMED)	I	8.74	1.22	1.55	2.03	3.55
OPTICAL PROPERTIES							
30	BEFORE REVERSION :						
	BRIGHTNESS (ISO-457nm)	I	62.5	71.7	75.7	77	78.9
	L*	-	88.1	93.7	94.5	94.9	95.2
	A*	-	-8.37	-1.85	-2.15	-2.31	-2.88
	B*	-	9.23	10.91	9.18	8.87	8.82
AFTER REVERSION :							
35	BRIGHTNESS (ISO-457nm)	I	61.9	71.3	74.7	76.2	78.2
	L*	-	88.0	93.5	94.4	94.7	95.1
	A*	-	-8.37	-2.19	-2.38	-1.81	-1.93
	B*	-	9.64	11.36	9.69	9.86	9.83

1 TABLE 6: CHEMICAL CHARGES AND BLEACHING CONDITIONS FOR
THE SEQUENCE SODIUM HYDROSULFITE-PEROXIDE-PEROXIDE (HPP)

FIRST STAGE							
5	D.T.P.A.	z	0.48	0.48	0.48	0.48	0.48
	H2O2 ADDED	z	1.88	1.88	1.88	1.88	1.88
	CONSISTENCY	z	5.8	5.8	5.8	5.8	5.8
	TEMPERATURE	c	78	78	78	78	78
	RETENTION TIME	hr.	0.5	0.5	0.5	0.5	0.5
	PH (INITIAL)	-	5.4	5.5	5.4	5.4	5.3
	PH (FINAL)	-	5.1	5.1	5.0	4.9	5.8
SECOND STAGE							
10	Na2S103	z	3.88	3.88	3.88	3.88	3.88
	MgSO4	z	0.85	0.85	0.85	0.85	0.85
	NaOH	z	1.39	1.39	1.57	1.74	2.26
	D.T.P.A.	z	0.48	0.48	0.48	0.48	0.48
	H2O2 ADDED	z	0.58	1.00	1.58	2.58	4.00
	CONSISTENCY	z	10.0	10.0	10.0	10.0	10.0
	TEMPERATURE	c	78	78	78	78	78
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5
	PH (INITIAL)	-	11.1	11.0	11.0	10.9	10.9
	PH (FINAL)	-	9.5	9.1	9.8	8.7	8.8
THIRD STAGE							
15	Na2S103	z	3.88	3.88	3.88	3.88	3.88
	MgSO4	z	0.85	0.85	0.85	0.85	0.85
	NaOH	z	1.08	1.25	1.25	1.75	2.00
	D.T.P.A.	z	0.48	0.48	0.48	0.48	0.48
	H2O2 ADDED	z	0.58	1.00	1.58	2.58	4.00
	CONSISTENCY	z	20.0	20.0	20.0	20.0	20.0
	TEMPERATURE	c	78	78	78	78	78
	RETENTION TIME	hr.	1.5	1.5	1.5	1.5	1.5
	PH (INITIAL)	-	11.1	11.0	10.9	11.1	11.1
	PH (FINAL)	-	10.2	10.2	9.9	10.5	10.6
TOTAL							
20	H2O2 (ADDED)	z	1.88	2.88	3.88	5.00	8.00
	H2O2 (RESIDUAL)	z	0.19	0.81	1.68	2.79	3.56
	H2O2 (CONSUMED)	z	0.81	1.19	1.48	2.21	2.44
OPTICAL PROPERTIES							
30	BEFORE REVERSION :						
	BRIGHTNESS (180-457nm)	z	62.5	71.4	75.7	76.8	79.8
	L*	-	88.1	93.4	94.5	94.5	95.0
	A*	-	-0.37	-2.08	-1.85	-1.66	-1.97
	B*	-	9.25	10.81	9.17	8.45	7.49
35	AFTER REVERSION :						
	BRIGHTNESS (180-457nm)	z	61.9	78.4	74.7	75.7	77.7
	L*	-	88.8	93.1	94.4	94.4	94.8
	A*	-	-0.37	-1.87	-1.93	-1.59	-1.88
	B*	-	9.64	11.04	9.69	8.95	8.88

1 CLAIMS

1. A process for the bleaching of mechanical and chemimechanical pulps which includes the steps of
5 treating in a first stage the pulp with a reducing agent and subsequently treating the same pulp with a peroxygen compound in a second stage followed by a subsequent treatment with a peroxygen compound in a third stage.
- 10 2. The process of claim 1 in which the reducing agent is sodium hydrosulfite.
- 15 3. The process of claim 2 in which treatment of the pulp in the first stage utilizes a chemical charge of 0.75 to 1.25% sodium hydrosulfite by weight of oven dried pulp in the presence of a chelating agent at a reaction temperature between 65 to 85°C, a consistency between 3.5 to 5%, a reaction time between 1 and 40 minutes and a reaction terminating pH of about 4.5 to 5.0.
- 20 4. The process of claim 3 in which following the first stage bleaching with a reducing agent the pulp is dewatered and washed to remove unreacted reducing agents and by-products.
- 25 5. The process of claim 4 in which 3 to 10% of peroxygen by weight of oven dried pulp is dispersed into the pulp using a mixer and transferring the pulp and bleaching fluid to a bleaching tower.
- 30 6. The process of claim 5 in which sodium hydroxide, sodium silicate and magnesium sulfate are added to stabilize the peroxygen compound in ranges of 0.5 - 3.0%, 0.0 to 3.0% and 0.01 to 0.05% respectively.
7. The process of claim 6 in which small amounts of DTPA between 0.1 - 0.4% are added to the bleach fluid.

1 8. The process of claim 7 in which the consistency of
the pulp is in the 10 - 12% range, the temperature is 65
- 70°C and the retention time is 60 to 90 minutes.

5 9. The process of claim 8 in which the pulp from the
first bleaching tower is dewatered and washed to remove
the by-products produced from the bleaching reactions.

10 10. The process of claim 9 in which 3 to 10% of
peroxygen by weight of oven dried pulp is dispersed into
the pulp using a mixer and the pulp and bleaching fluid
are transferred to a bleaching tower.

15 11. The process of claim 10 in which sodium hydroxide,
sodium silicate and magnesium silicate are added to
stabilize the peroxygen compound in ranges of 0.5 - 3.0%,
0.0 to 3.0% and 0.01 to 0.05% respectively.

20 12. The process of claim 11 in which the consistency
of the pulp is in the range from 20 - 35%, and primarily
fresh peroxygens are mixed with the pulp.

25 13. The process of claim 12 in which the pulp is
washed and dewatered following the third stage bleaching.

14. The process of claim 13 in which sulfuric acid is
added to the pulp after washing and dewatering to lower
the aqueous solution pH to about 6.

30 15. The process of claim 1 in which the reducing agent
is sodium borohydride.

35 16. The process of claim 15 in which treatment of the
pulp in the first stage utilizes a chemical charge of 0.3
to 0.5% of sodium borohydride by weight of oven dried
pulp in the presence of a chelating agent at a reaction
temperature between 65 to 85°C, a consistency between 10
and 12%, a reaction time between 1 to 40 minutes and a
reaction terminating pH of 10.0 to 10.5.

- 1 17. The process of claim 16 in which following the first stage bleaching with a reducing agent the pulp is dewatered and washed to remove unreacted reducing agents and by-products.
- 5 18. The process of claim 17 in which 3 to 10% of peroxygen by weight of oven dried pulp is dispersed into the pulp using a mixer and transferring the pulp and bleaching fluid to a bleaching tower.
- 10 19. The process of claim 18 in which sodium hydroxide, sodium silicate and magnesium sulfate are added to stabilize the peroxygen compound in ranges of 0.5 - 3.0%, 0.0 to 3.0% and 0.01 to 0.05% respectively.
- 15 20. The process of claim 19 in which small amounts of DTPA between 0.1 - 0.4% are added to the bleach fluid.
- 20 21. The process of claim 20 in which the consistency of the pulp is in the 10 - 12% range, the temperature is 65 - 70°C and the retention time is 60 to 90 minutes.
- 25 22. The process of claim 21 in which the pulp from the second stage bleaching tower is dewatered and washed to remove the by-products produced from the bleaching reactions.
- 30 23. The process of claim 22 in which 3 to 10% of peroxygen by weight of oven dried pulp is dispersed into the pulp using a mixer and the pulp and bleaching fluid are transferred to a bleaching tower.
- 35 24. The process of claim 23 in which sodium hydroxide, sodium silicate and magnesium silicate are added to stabilize the peroxygen compound in ranges of 0.5 - 3.0%, 0.0 to 3.0% and 0.01 to 0.05% respectively.
25. The process of claim 24 in which the consistency of the pulp is in the range from 20 - 35%, and primarily fresh peroxygens are mixed with the pulp.

- 1 26. The process of claim 25 in which the pulp is washed and dewatered following the third stage bleaching.
- 5 27. The process of claim 26 in which sulfuric acid is added to the pulp after washing and dewatering to lower the aqueous solution pH to about 6.
- 10 28. The process of claim 1 characterized by the reducing compound being selected from the group consisting of sodium bisulfite, magnesium bisulfite, zinc hydrosulfite, BOROL, thiurea dioxide, ammonium borohydride and hydrazine.
- 15 29. The process of claim 1 in which the treatment of the pulp with the reducing agent utilizes a charge of about 0.01 to about 1.5% by weight in the presence of a chelating agent at a reaction temperature of between 60°C to 100°C for a time of between 4 to 120 minutes at a pulp consistency of from 3% to 35% and a reaction terminating pH of between 3.5 to about 11.0; the process being further characterized by washing said pulp after treatment.
- 25 30. The process of claim 29 characterized by the peroxygen compound being selected from the group consisting of hydrogen peroxide, sodium peroxide, benzyl peroxide, ditertiarybutyl peroxide and peracetic acid.
- 30 31. The process of claim 30 in which the treatment of the pulp with a peroxygen compound in the second stage utilizes a charge of between 0.01% to about 5.0% by weight at a temperature of between 60°C to 100°C for a time period of between 4 minutes to 180 minutes at a pulp consistency of between 4% to about 40% and a reaction terminating pH of between 0.5 to 10.5.
- 35 32. The process of claim 31 in which the treatment with said peroxygen compound in the third stage utilizes a charge of between 0.1 to about 12% by weight based on oven dried pulp at a temperature of between 60°C to 100°C

- 1 for a period of from 4 minutes to 250 minutes at a pulp consistency of between 4% and 40% and a reaction terminating pH of from 7.5 to about 10.0.
- 5 33. The process of claim 32 characterized by the peroxygen compounds being selected from the group consisting of sodium peroxide, benzyl peroxide, ditertiarybutyl peroxide and peracetic acid.
- 10 34. The process of claim 33 characterized by the treatment of the pulp with the peroxygen compounds being carried out in the presence of sodium hydroxide, sodium silicate, magnesium sulfate and DTPA.
- 15 35. The process of claim 1 characterized by the pulp being selected from the group of pulps consisting of high yield and ultra high yield pulps which are referred to as mechanical, chemimechanical, chemithermomechanical, groundwood, high-yield or ultra high yield sulfite pulps.

112

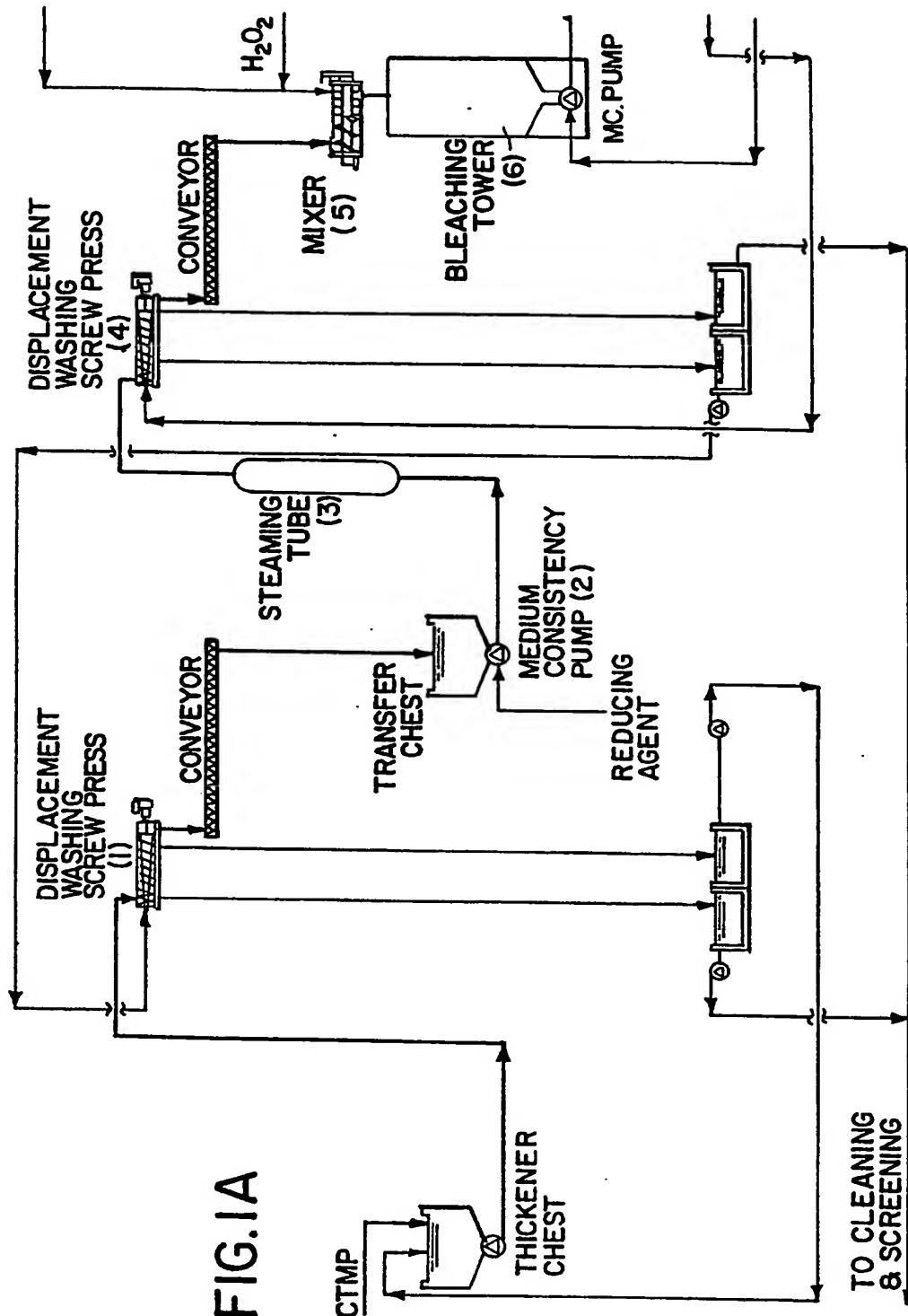
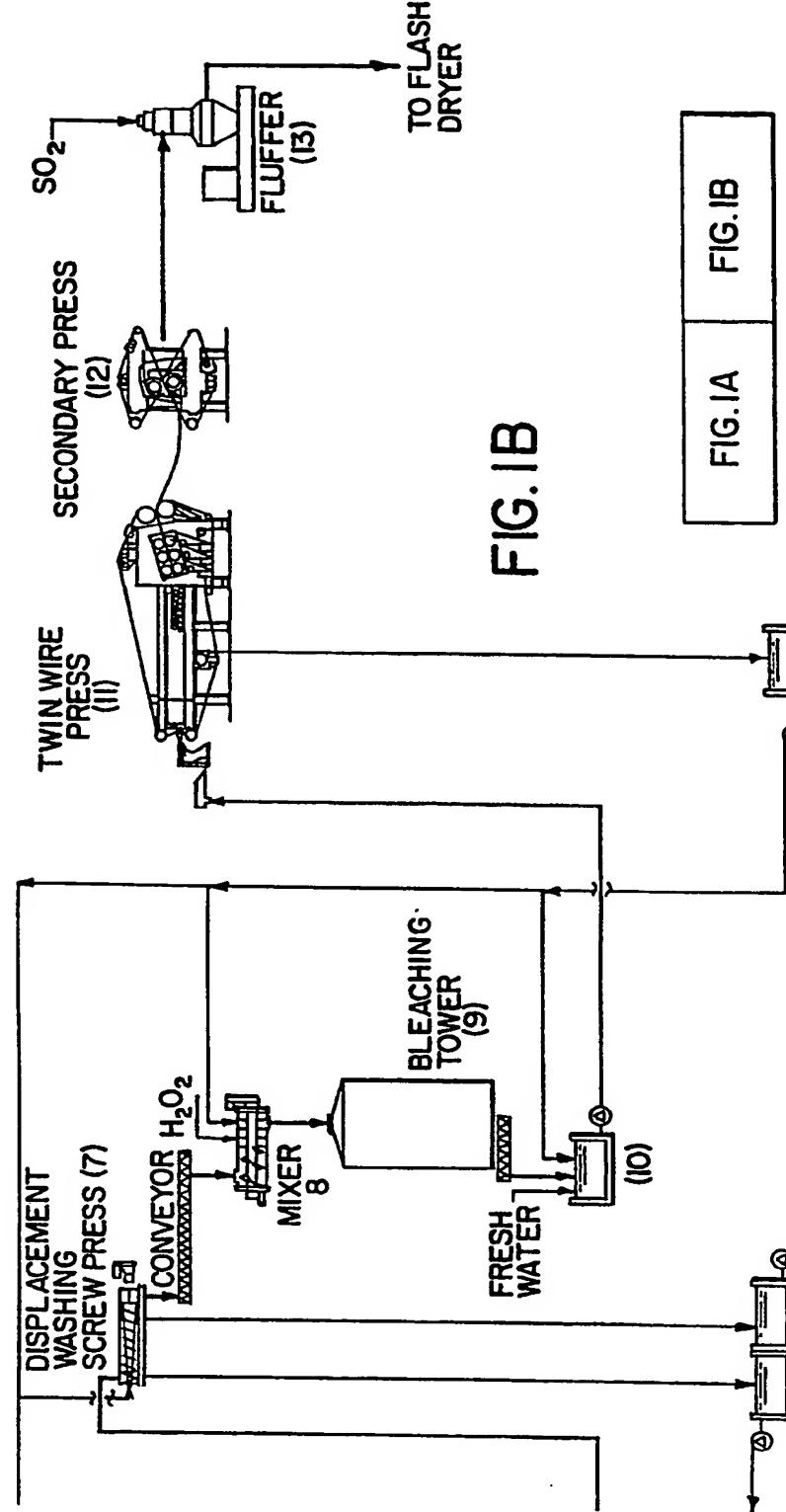


FIG. I.A

2 / 2



INTERNATIONAL SEARCH REPORT

International Application No

PCT/CA 90/00097

I. CLASSIFICATION OF SUBJECT MATTER (If several classification symbols apply, indicate all)⁶

According to International Patent Classification (IPC) or to both National Classification and IPC

Int.C1. 5 D21C9/10

II. FIELDS SEARCHED

Minimum Documentation Searched⁷

Classification System	Classification Symbols
Int.C1. 5	D21C

Documentation Searched other than Minimum Documentation
to the Extent that such Documents are Included in the Fields Searched⁸III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹

Category ¹⁰	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
Y	EP,A,0187477 (PULP AND PAPER RESEARCH INSTITUTE OF CANADA) 16 July 1986 see the whole document (cited in the application) ---	1-11, 14-24, 27-35
Y	BULLETIN OF THE INSTITUTE OF PAPER CHEMISTRY. vol. 53, no. 2, August 1982, APPLETON US page 260 M.YOTSUYA et al.: "Peroxide bleaching of high-yield pulp." see the whole document ---	1-11, 14-24, 27-35
A	EP,A,0191756 (KAMYR AB) 20 August 1986 see the whole document (cited in the application) ----	

¹⁰ Special categories of cited documents :¹⁰

"A" document defining the general state of the art which is not considered to be of particular relevance
 "E" earlier document but published on or after the international filing date
 "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
 "O" document referring to an oral disclosure, use, exhibition or other means
 "P" document published prior to the international filing date but later than the priority date claimed

"I" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step

"V" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"R" document member of the same patent family

IV. CERTIFICATION

Date of the Actual Completion of the International Search

1 20 JULY 1990

Date of Mailing of this International Search Report

16 AOUT 1990

International Searching Authority

EUROPEAN PATENT OFFICE

Signature of Authorized Officer

SONGY O. M-L. A.

ANNEX TO THE INTERNATIONAL SEARCH REPORT
ON INTERNATIONAL PATENT APPLICATION NO.

CA 90/00097
SA 35818

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

20/07/90

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP-A-0187477	16-07-86	CA-A- 1249402 JP-A- 61186593 US-A- 4804440	31-01-89 20-08-86 14-02-89
EP-A-0191756	20-08-86	JP-A- 61245392 SE-A- 8600615	31-10-86 16-08-86